

# Ciclo di STIRLING

- 2 isoterme a  $T_1 = 310\text{K}$ ,  $T_2 = 500\text{K}$
- 2 isocore a  $V_A = 0.002\text{m}^3$ ,  $V_B = 0.004\text{m}^3$

Gas monoatomico

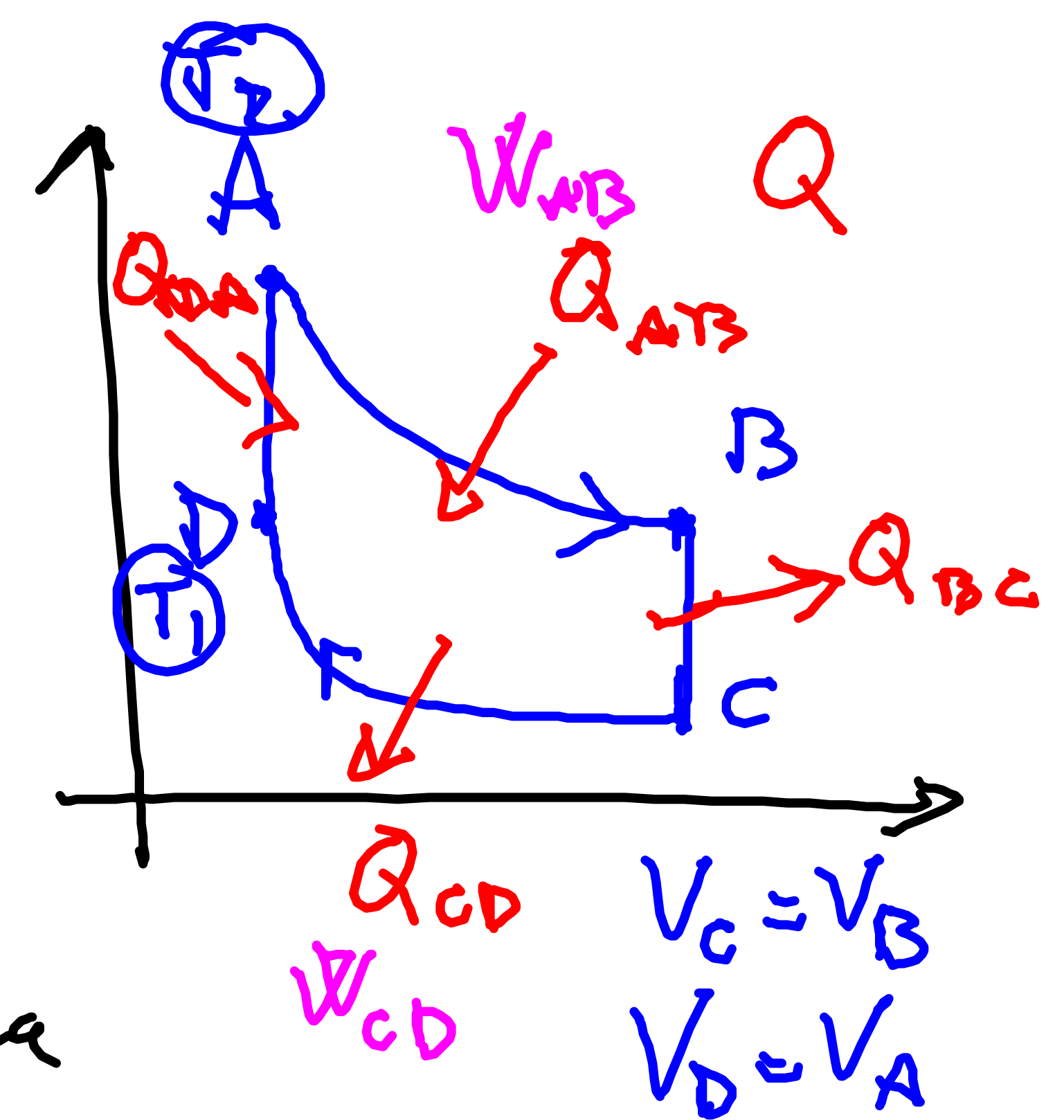
Determinare il rendimento

- nel caso il ciclo sia reversibile
- nel caso vi siano due sole sorgenti di temperatura

$$a) \eta_{\text{max}} = \eta_{\text{Carnot}} = 1 - \frac{T_1}{T_2} = 1 - \frac{310}{500} = 0.38 \checkmark$$

$$b) \eta = \frac{W}{Q_{\text{fornite}}} = \frac{W_{AB} + W_{CD}}{Q_{AB} + Q_{DA}} = \frac{Q_{AB} + Q_{CD}}{Q_{AB} + Q_{DA}}$$

$$Q_{AB} = W = nRT_2 \ln(V_B/V_A) = nRT_2 \ln 2$$



$Q_{DA}$  viene fornita dal trasferimento di calore da  $T_2$  a  $T_1$

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invece:  $W=0 \rightarrow Q = +\Delta U$   
 $Q = nC_v(T_2 - T_1) = U_f - U_i$   
 $= nC_v T_2 - nC_v T_1$

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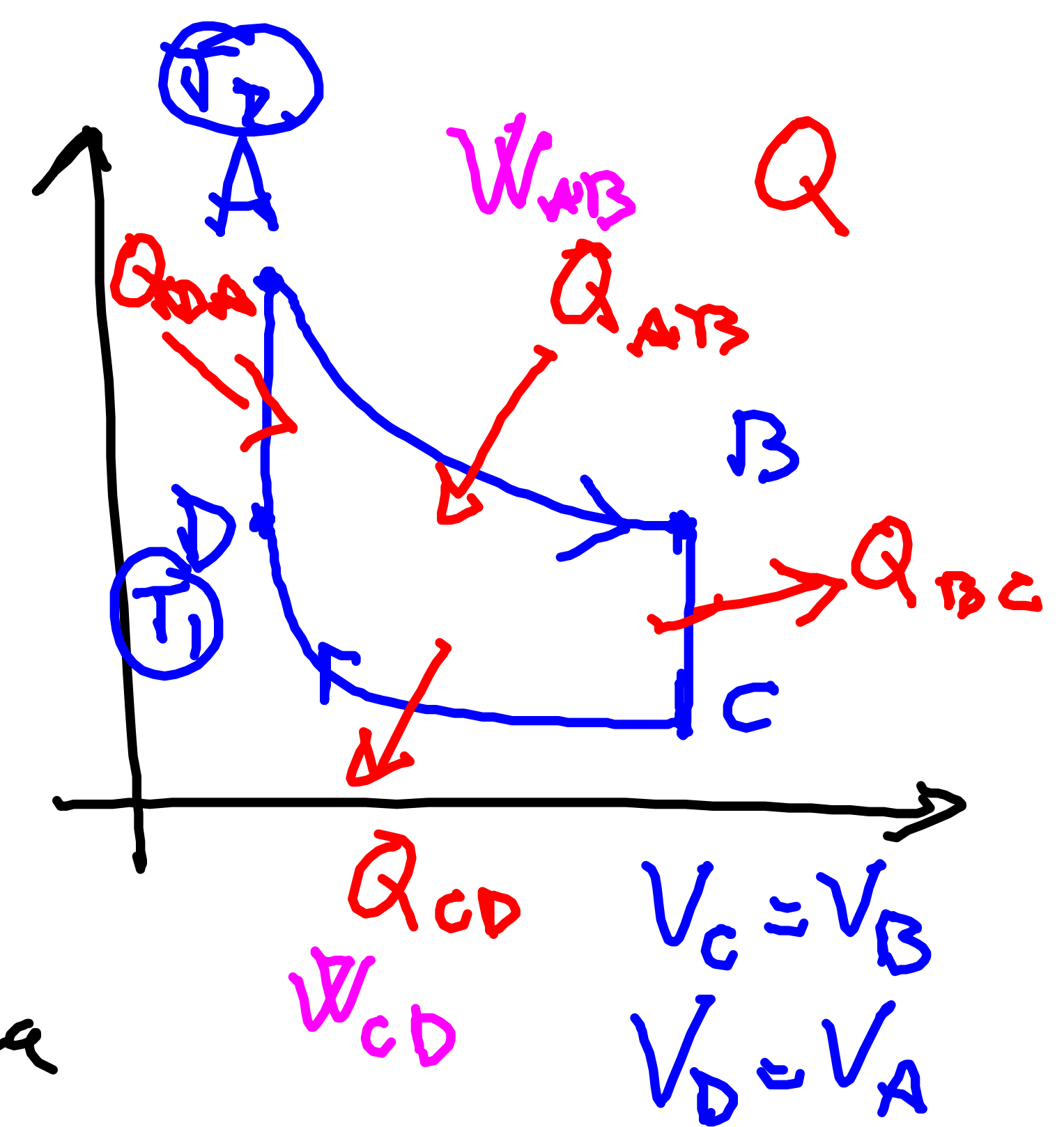
Determinare il rendimento

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$$Q_{AB} = nRT_2 \ln 2$$

$$Q_{CD} = nRT_1 \ln \frac{V_D}{V_C} = nRT_1 \ln \frac{1}{2} = -nRT_1 \ln 2$$

$$\eta = \frac{Q_{AB} + Q_{CD}}{Q_{AB} + Q_{DA}} = \frac{nRT_2 \ln 2 - nRT_1 \ln 2}{nRT_2 \ln 2 - nC_V(T_2 - T_1)} = \frac{(T_2 - T_1) \ln 2}{T_2 \ln 2 - \frac{3}{2}(T_2 - T_1)} = 0.27$$



# Ciclo OTTO

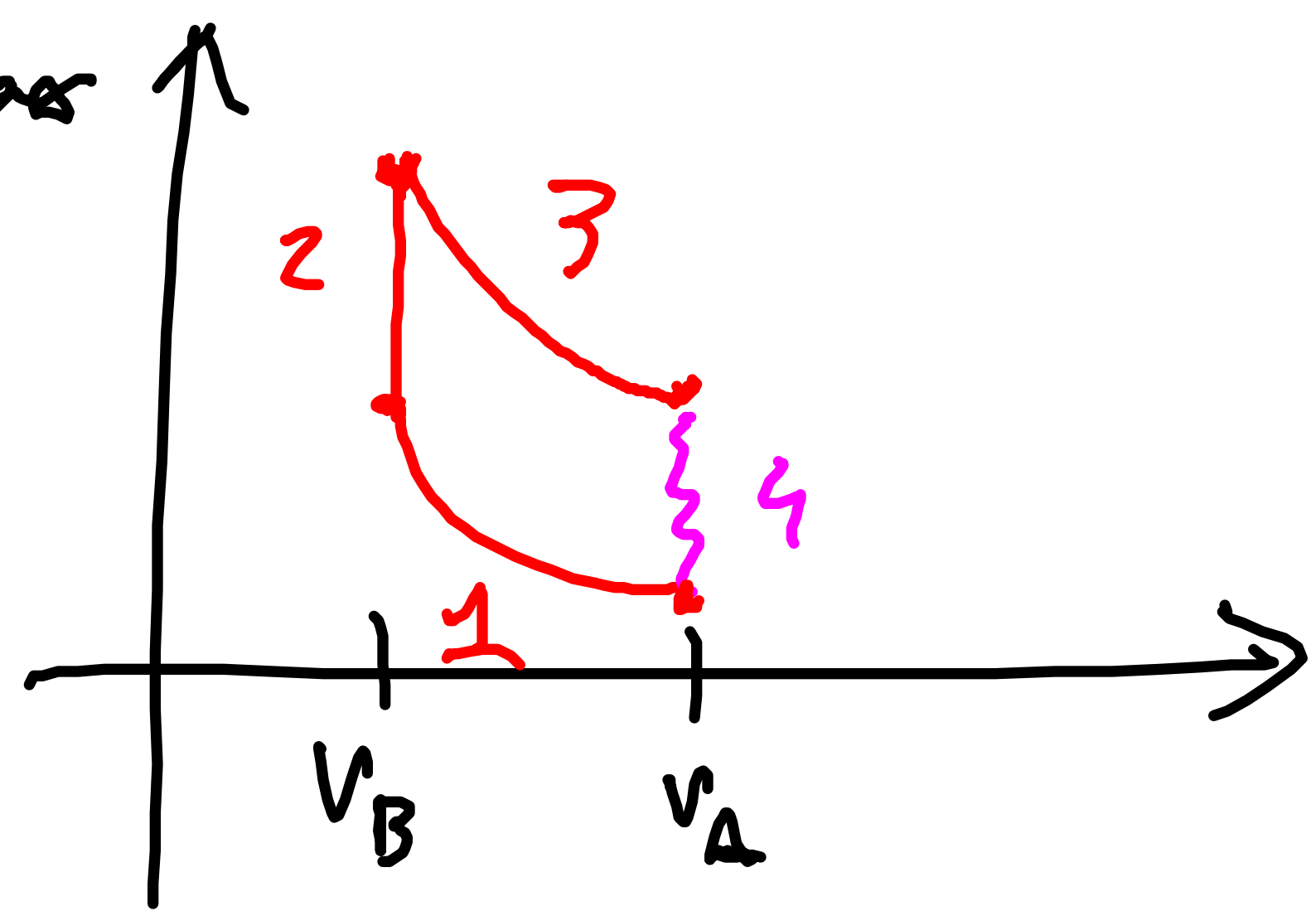
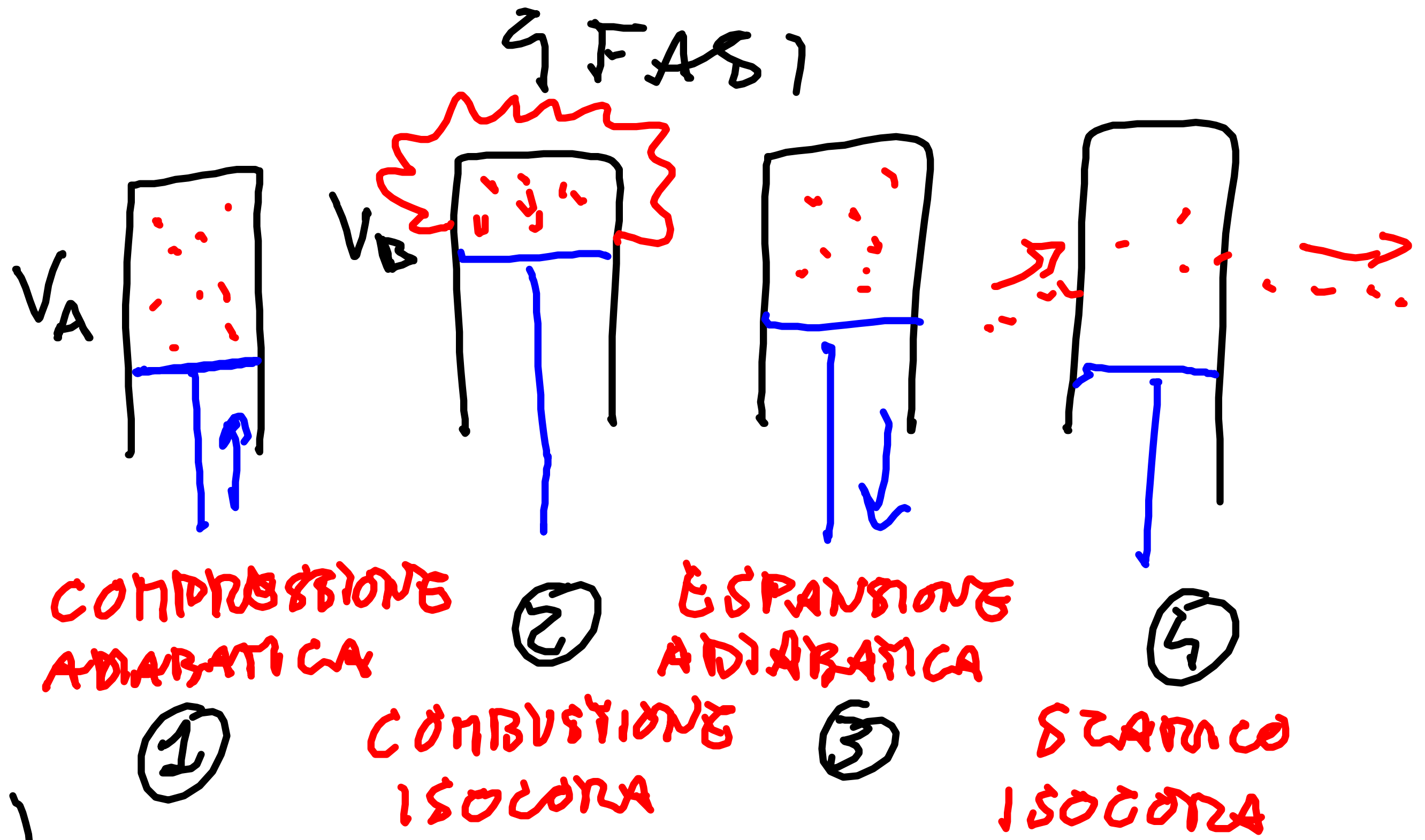
Ciclo dei motori a combustione

rapporto di compressione

$$\frac{V_A}{V_B} = 6, \quad \gamma = 1.3$$

$$T_A = 300 \text{ K}, \quad T_C = 1200 \text{ K}$$

- a)  $T_B = ?$    b)  $T_D = ?$    c)  $\eta = ?$    d)  $\eta_{max}$



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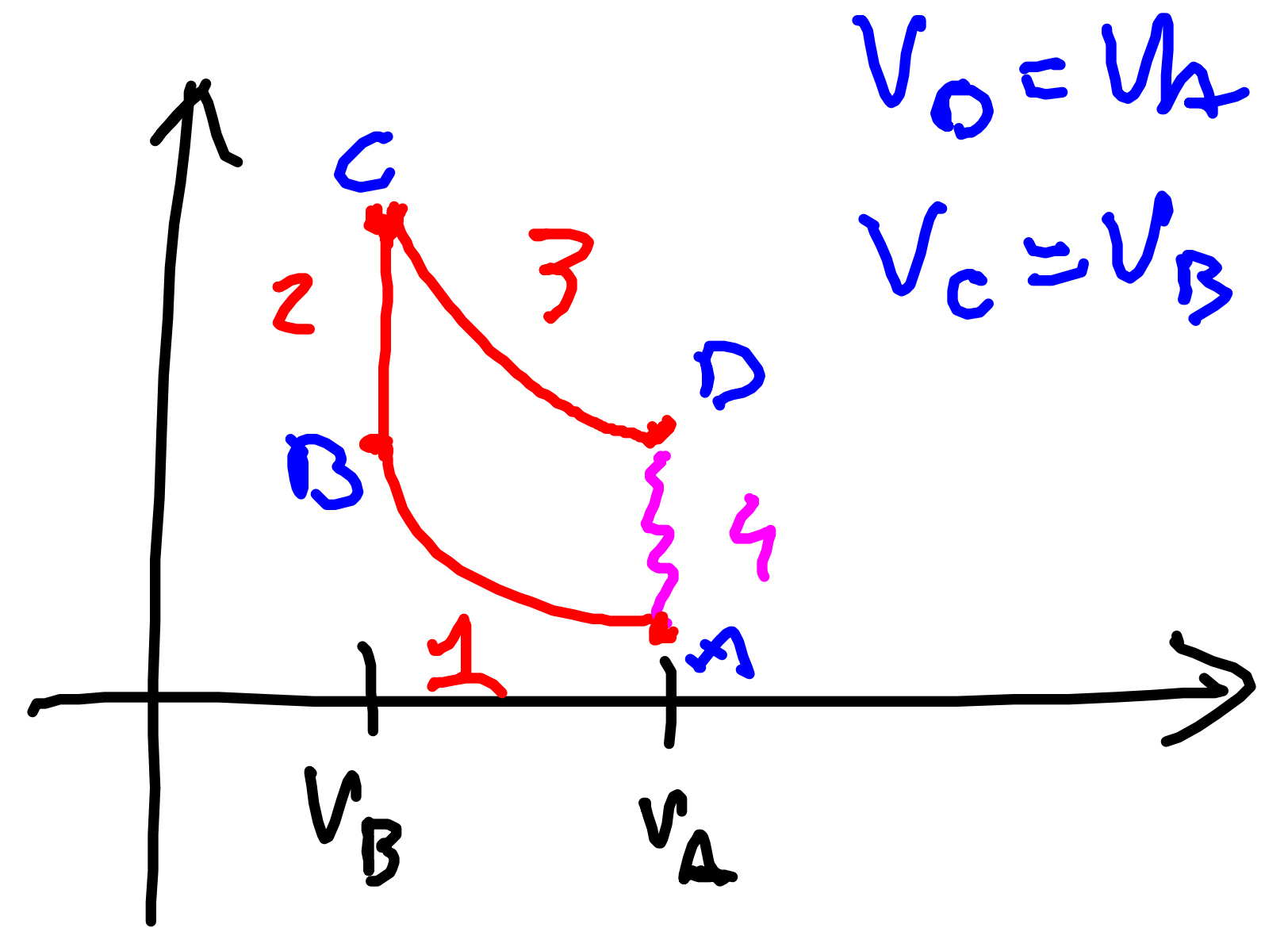
a)  $T_B = ?$  b)  $T_D = ?$  c)  $\eta = ?$  d)  $\eta_{\text{max}}$

a)  $A \rightarrow B$  adiabatica  $pV^\gamma = \text{cost}$

$$P_A V_A^\gamma = P_B V_B^\gamma \quad \text{includere } pV = nRT$$

$$T_A V_A^{\gamma-1} = T_B V_B^{\gamma-1}$$

$$T_B = T_A \left( \frac{V_A}{V_B} \right)^{\gamma-1} = 300 \cdot 6^{1.3-1} = 513 \text{ K}$$



b)  $C \rightarrow D$  adiabatica

$$T_C V_C^{\gamma-1} = T_D V_D^{\gamma-1}$$

$$T_D = T_C \left( \frac{V_C}{V_D} \right)^{\gamma-1}$$

$$= T_C \left( \frac{V_B}{V_A} \right)^{\gamma-1}$$

$$= 1200 \left( \frac{1}{6} \right)^{\gamma-1} = 701 \text{ K}$$

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a)  $T_B = ?$  b)  $T_D = ?$  c)  $\eta = ?$  d)  $\eta_{\text{max}}$

$$Q_1 = 0 \quad \text{adiab.}$$

$$Q_3 = 0$$

$$W_2 = 0$$

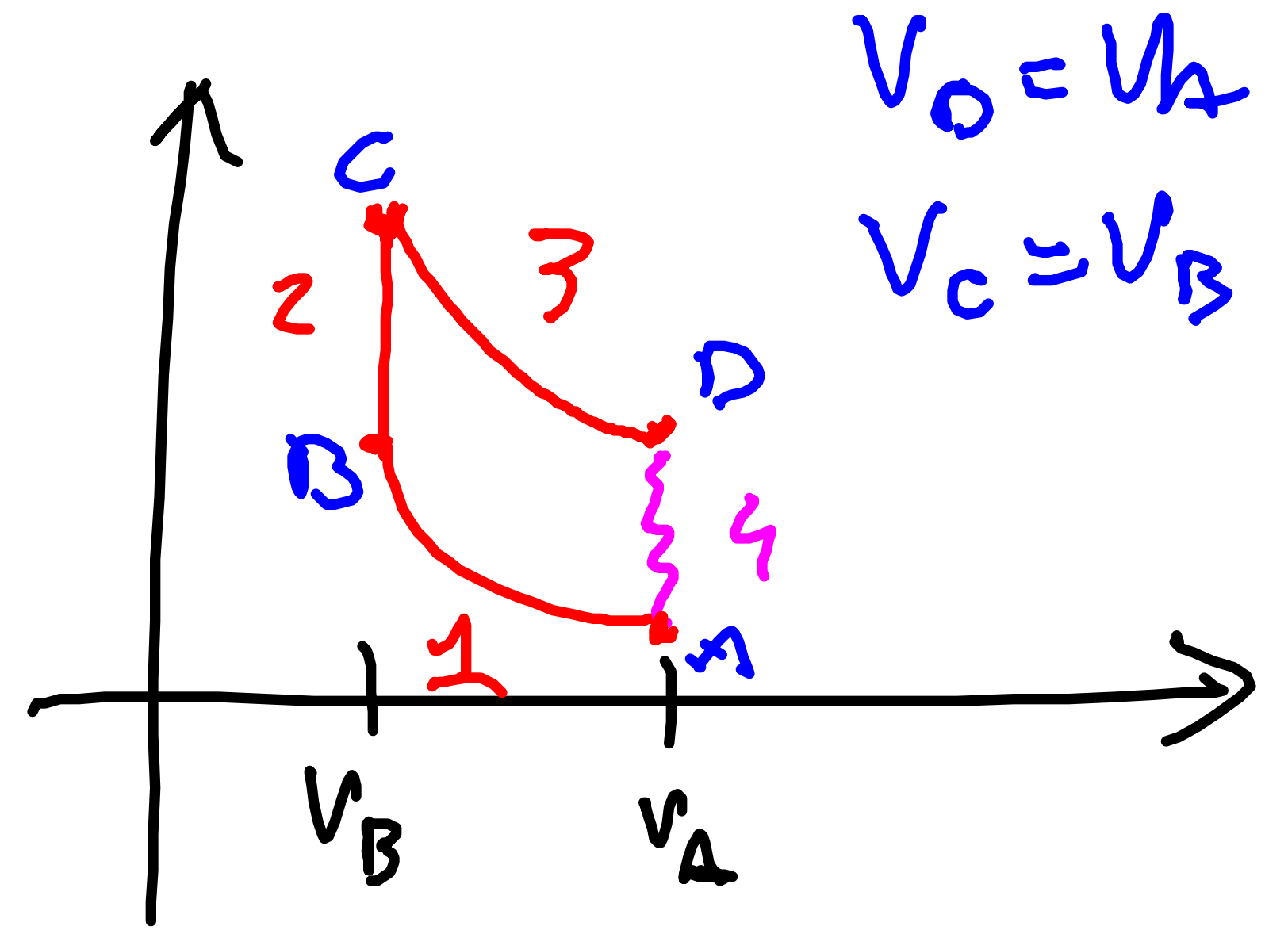
$$W_4 = 0$$

isocore

$$\eta = \frac{\text{lavoro}}{\text{calore fornito}} = \frac{Q_2 + Q_4}{Q_2} = \frac{m C_V (T_C - T_B) + m C_V (T_A - T_D)}{m C_V (T_C - T_B)}$$

$$= 1 + \frac{T_A - T_D}{T_C - T_B} = 0.42$$

$$\eta = 1 - \frac{T_{\text{min}}}{T_{\text{max}}} = 1 - \frac{T_A}{T_C} = 0.75$$



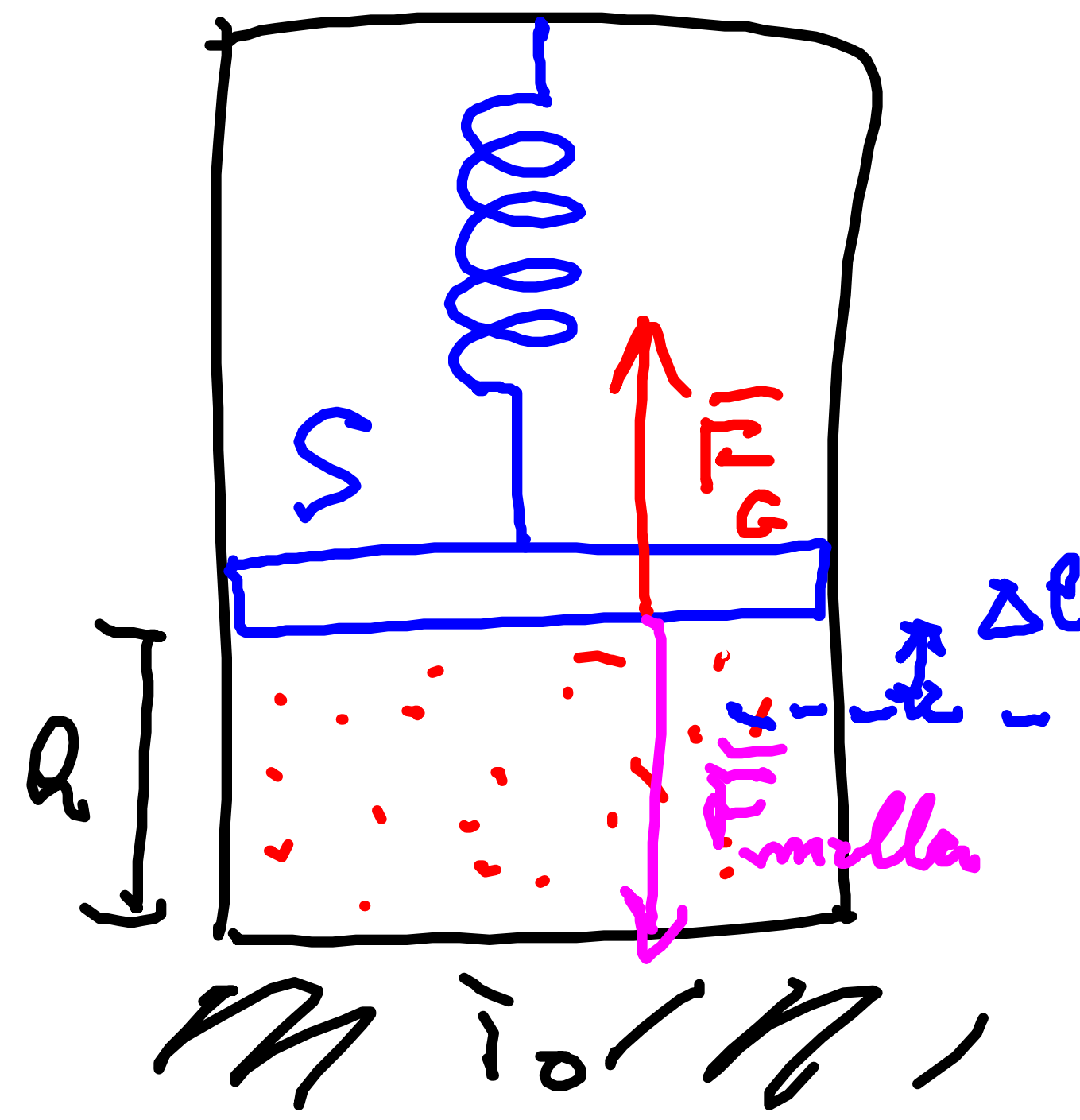
# Molla e pistone

Gas ideale monoatomico ( $n = 0.3 \text{ mol}$ )

$T_0 = 300 \text{ K}$ , è connesso ad un termistore all'inizio in equilibrio termico

$h = 20 \text{ cm}$ ,  $k_{\text{molla}} = 50000 \text{ N/m}$

Pompare al gas del calore finché la molla è compressa di un valore doppio di quello iniziale



a) compressione iniziale  $\Delta \ell = ?$  b)  $T_f = ?$  c)  $Q = ?$

$$a) \quad p = \frac{F}{S} \quad F_{\text{molla}} = pS = k\Delta \ell$$

$$k\Delta \ell = \frac{nRT_0}{V} S = \frac{nRT_0}{hS} S = \frac{nRT_0}{h} \quad \rightarrow \quad \Delta \ell = \frac{nRT_0}{k h} = 7.5 \text{ cm}$$

$$b) \quad p_f S = k(2\Delta \ell) = \frac{nRT_f}{V_f} S = \frac{nRT_f}{S(h+\Delta \ell)} \quad \rightarrow \quad T_f = \frac{2k\Delta \ell (h+\Delta \ell)}{nR} = 824 \text{ K}$$

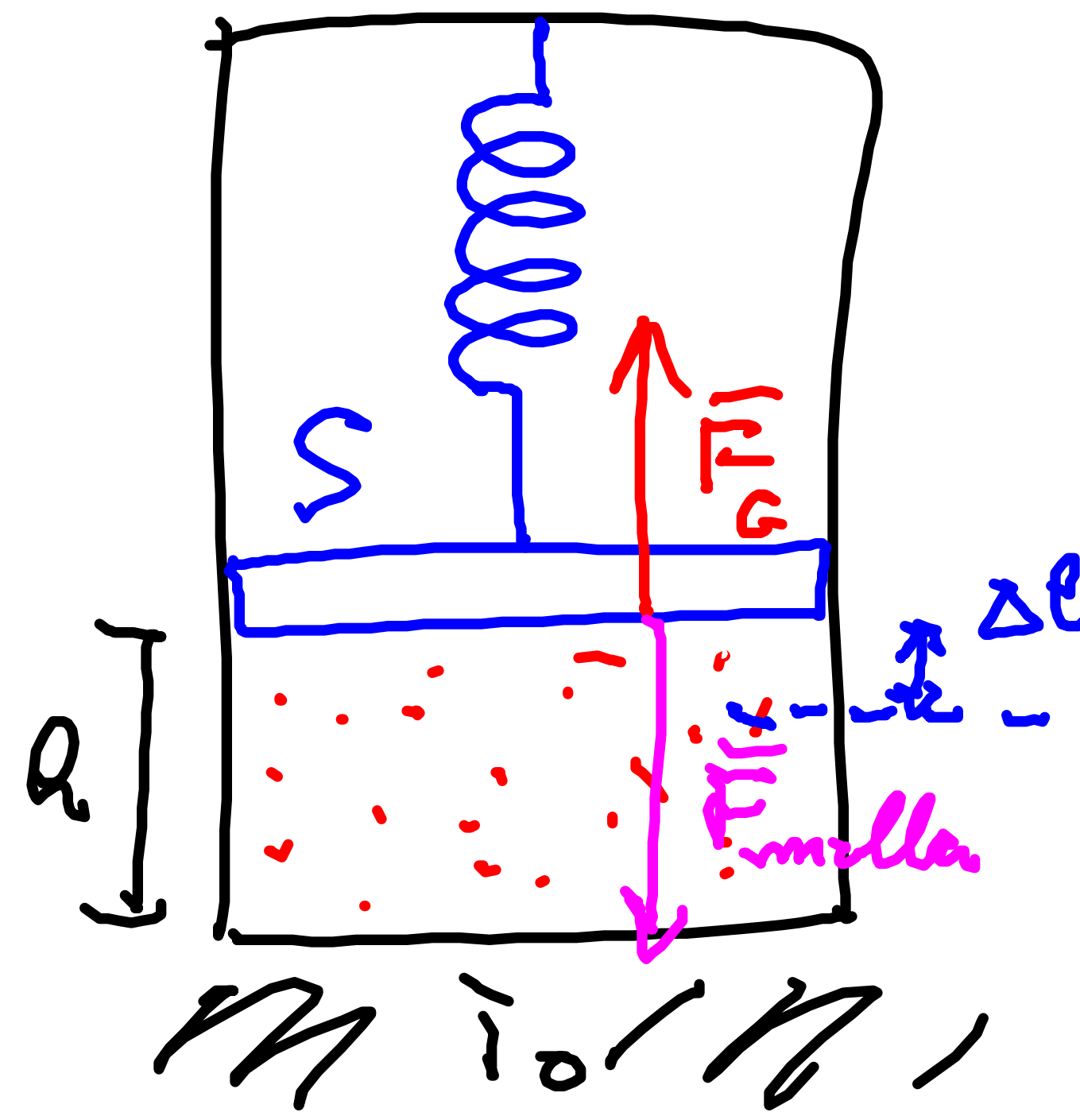
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a) compressione iniziale  $\Delta L = ?$  b)  $T_f = ?$  c)  $Q = ?$

c)  $Q = \Delta U + W$

$$W = \int_{\Delta L}^{2\Delta L} F dx = \int_{\Delta L}^{2\Delta L} kx dx = k \left[ \frac{x^2}{2} \right]_{\Delta L}^{2\Delta L} = \frac{1}{2} k (4\Delta L^2) - \frac{1}{2} k (\Delta L^2) = \frac{3}{2} k \Delta L^2 = 420 \text{ J}$$

$$\Delta U = U_f - U_i = n C_v T_f - n C_v T_0 \quad Q = n \frac{3}{2} R (T_f - T_0) + \frac{3}{2} k \Delta L^2 = 2.39 \times 10^3 \text{ J}$$

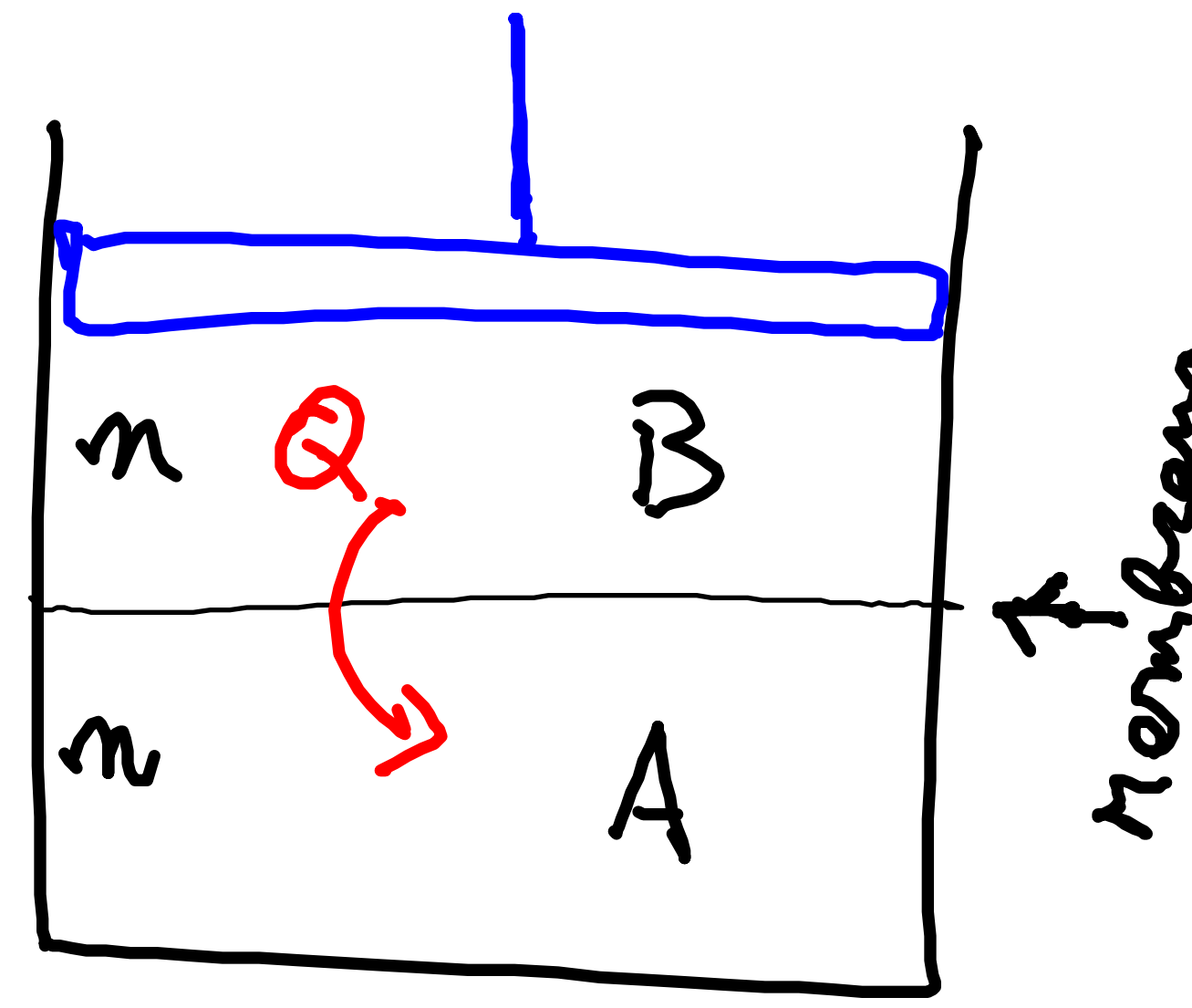
# Problema III 12/6/18

Cilindro a pareti isolate; chiuso da pistone  
 $n = 2 \text{ mol}$ , gas perfetto monoatomico

$T_i = 270 \text{ K}$

$V_B^p = \frac{1}{2} V_B$ ,  $T_p = 340 \text{ K}$

- a)  $\frac{P_B^i}{P_B^p} = ?$     b)  $W_{\text{sist}}$     c)  $\Delta S = ?$



a)  $P_B^i V_B = n R T_i$   
 $P_B^p V_B^p = n R T_p$   
 $\rightarrow \frac{P_B^i V_B}{T_i} = \frac{P_B^p V_B^p}{T_p} \rightarrow \frac{P_B^i}{P_B^p} = \frac{V_B^p}{V_B} \frac{T_i}{T_p} = \frac{1}{2} \frac{270}{340} = 0.39$

vale per TUTTO il sistema  
 $n = 4$

b) non ha Q  $\rightarrow \Delta U = Q - W = -W$

$U = n C_v T$

$W = -\Delta U = U_i - U_f = n \frac{3}{2} R (T_i - T_p) = -3.5 \times 10^3 \text{ J}$



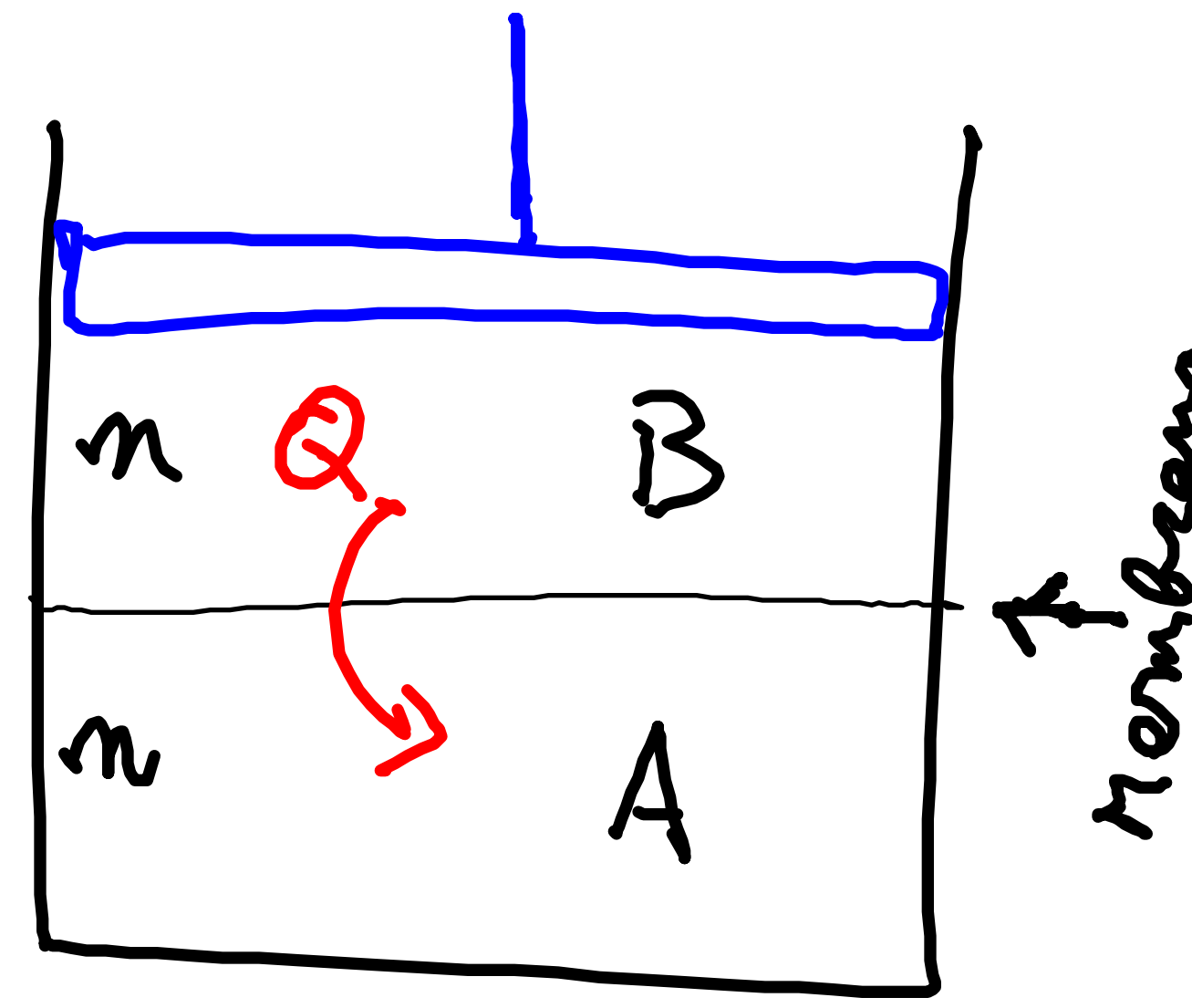
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- a)  $\frac{P_B^i}{P_B^f} = ?$     b)  $W_{\text{sist}}$     c)  $\Delta S = ?$



$$c) \Delta S = \Delta S_A + \Delta S_B = \int \frac{\delta Q_A}{T_A} + \int \frac{\delta Q_B}{T_B}$$

$$= \int \frac{\delta Q_A}{T_A} - \int \frac{\delta Q_A}{T_A} = 0$$

$T$  è uguale per entrambi  
 $T_A = T_B \forall t$

sistema isolato  
 $\delta Q_A = -\delta Q_B$